

**APPLICATION FOR UNITED STATES LETTERS PATENT**

**for**

**NESTED COMPACT FUEL PROCESSOR FOR PRODUCING A HYDROGEN  
RICH GAS**

**by**

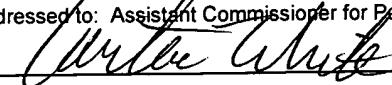
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## BACKGROUND OF THE INVENTION

2 Fuel cells provide electricity from chemical oxidation-reduction reactions and  
3 possess significant advantages over other forms of power generation in terms of  
4 cleanliness and efficiency. Typically, fuel cells employ hydrogen as the fuel and oxygen  
5 as the oxidizing agent. The power generation is proportional to the consumption rate of  
6 the reactants.

7 A significant disadvantage which inhibits the wider use of fuel cells is the lack of  
8 a widespread hydrogen infrastructure. Hydrogen has a relatively low volumetric energy  
9 density and is more difficult to store and transport than the hydrocarbon fuels currently  
10 used in most power generation systems. One way to overcome this difficulty is the use of  
11 reformers to convert the hydrocarbons to a hydrogen rich gas stream which can be used  
12 as a feed for fuel cells.

13 Hydrocarbon-based fuels, such as natural gas, LPG, gasoline, and diesel, require  
14 conversion processes to be used as fuel sources for most fuel cells. Current art uses multi-  
15 step processes combining an initial conversion process with several clean-up processes.  
16 The initial process is most often steam reforming (SR), autothermal reforming (ATR),  
17 catalytic partial oxidation (CPOX), or non-catalytic partial oxidation (POX). The clean-  
18 up processes are usually comprised of a combination of desulfurization, high temperature  
19 water-gas shift, low temperature water-gas shift, selective CO oxidation, or selective CO  
20 methanation. Alternative processes include hydrogen selective membrane reactors and  
21 filters.

22 Despite the above work, there remains a need for a simple unit for converting a  
23 hydrocarbon fuel to a hydrogen rich gas stream for use in conjunction with a fuel cell.

24

## 25 SUMMARY OF THE INVENTION

26 The present invention is generally directed to an apparatus and method for  
27 converting hydrocarbon fuel into a hydrogen rich gas. In one illustrative embodiment of  
28 the present invention, the apparatus for converting hydrocarbon fuel into hydrogen rich  
29 gas includes a plurality of modules arranged radially along a common axis. Such an  
30 arrangement permits a compact design and highly efficient heat transfer between  
31 differing reactor modules. Depending upon the reaction taking place within the module,

1 each module may include an annular layer of thermally insulating material disposed  
2 between the shell and the respective processing core. In a similar manner, a module may  
3 include a porous support member, such as screen, mesh, perforated plate, or porous  
4 sintered plate. Such a porous support member may be included so as to support and  
5 contain the contents of the module, particularly granular catalyst materials.

6 As noted above and described herein, the apparatus of the present invention is  
7 used to carry out a series of reactions that converts hydrocarbon fuel to hydrogen rich  
8 gas. In one illustrative embodiment of such an apparatus, the first module preferably has  
9 a processing core that includes a partial oxidation catalyst or alternatively a steam  
10 reforming catalyst or alternatively an autothermal reforming catalyst or alternatively  
11 combinations and/or mixtures of such catalysts. A second module positioned adjacent to  
12 the first module is preferably designed so that the processing core of the second module  
13 includes a first heat exchanger. Such a heat exchanger may be a fin-typed heat  
14 exchanger, tubing heat exchanger, heat pipe, or similar means that are capable of  
15 exchanging heat.

16 Within the plurality of modules, a third module is preferably positioned adjacent  
17 to the second module, the processing core of the third module including a desulfurizing  
18 agent. A wide variety of desulfurizing agents may be used but preferably the  
19 desulfurizing agent includes zinc oxide. A fourth module positioned adjacent to and in  
20 fluid communication with the third module includes a processing core containing a water  
21 gas shift catalyst. One of skill in the art should understand and appreciate that the water  
22 gas shift catalyst may be a low temperature water gas shift catalyst that includes a  
23 catalyst material selected from copper, copper oxide, zinc, platinum, rhenium, palladium,  
24 rhodium, and gold and combinations and mixtures of these and similar materials.  
25 Alternatively, the water gas shift catalyst is a high temperature water gas shift catalyst  
26 that includes a catalyst material selected from ferric oxide, chromic oxide, copper, iron  
27 silicide, platinum, palladium and other platinum group members, and combinations and  
28 mixtures of these and similar materials.

29 The apparatus is further designed to include within the plurality of modules a fifth  
30 module positioned adjacent to and in fluid communication with the fourth module. The  
31 processing core of the fifth module includes a second heat exchanger. Such a heat

1       exchanger may include a fin-typed heat exchanger, tubing heat exchanger, heat pipe, or  
2       similar means that are capable of exchanging heat.

3       The plurality of modules further includes a sixth module positioned adjacent to  
4       the fifth module with which it is in fluid communication. The processing core of the sixth  
5       module includes a carbon monoxide oxidation catalyst that preferably includes a material  
6       selected from platinum, palladium, iron, chromium, manganese, iron oxide, chromium  
7       oxide, manganese oxide, ruthenium, gold, cerium, lanthanum, and combinations and  
8       mixtures of these and similar compounds.

9       The present invention also includes a process for converting hydrocarbon fuel into  
10      a hydrogen rich gas. One such illustrative process utilizes the apparatus disclosed herein.  
11      Such a process generally includes providing a fuel processor having a plurality of  
12      modules arranged radially along a common axis, each forming an annular reaction  
13      chamber. By feeding the hydrocarbon fuel successively through each of the above  
14      described modules in an generally radial direction a hydrogen rich gas is produced in a  
15      manner that optimizes space considerations and heat transfer considerations.

16

#### 17                    **BRIEF DESCRIPTION OF THE DRAWINGS**

18       The description is presented with reference to the accompanying drawings in  
19       which:

20       FIG. 1 depicts a simple process flow diagram for one illustrative embodiment of  
21       the present invention.

22       FIG. 2 depicts a first illustrative embodiment of a compact fuel processor  
23       apparatus of the present invention; and

24       FIG. 3 depicts a second illustrative embodiment of a compact fuel processor  
25       apparatus of the present invention.

26

#### 27                    **DESCRIPTION OF ILLUSTRATIVE EMBODIMENTS**

28       The present invention is generally directed to an apparatus for converting  
29       hydrocarbon fuel into a hydrogen rich gas. In a preferred aspect, the apparatus and  
30       method described herein relate to a compact processor for producing a hydrogen rich gas  
31       stream from a hydrocarbon fuel for use in fuel cells. However, other possible uses are

1 contemplated for the apparatus and method described herein, including any use wherein a  
2 hydrogen rich stream is desired. Accordingly, while the invention is described herein as  
3 being used in conjunction with a fuel cell, the scope of the invention is not limited to such  
4 use.

5 Each of the illustrative embodiments of the present invention describe a fuel  
6 processor or a process for using such a fuel processor with the hydrocarbon fuel feed  
7 being directed through the fuel processor. The hydrocarbon fuel may be liquid or gas at  
8 ambient conditions as long as it can be vaporized. As used herein the term  
9 "hydrocarbon" includes organic compounds having C-H bonds which are capable of  
10 producing hydrogen from a partial oxidation or steam reforming reaction. The presence  
11 of atoms other than carbon and hydrogen in the molecular structure of the compound is  
12 not excluded. Thus, suitable fuels for use in the method and apparatus disclosed herein  
13 include, but are not limited to hydrocarbon fuels such as natural gas, methane, ethane,  
14 propane, butane, naphtha, gasoline, and diesel fuel, and alcohols such as methanol,  
15 ethanol, propanol, and the like.

16 The fuel processor feeds include hydrocarbon fuel, oxygen, and water. The  
17 oxygen can be in the form of air, enriched air, or substantially pure oxygen. The water  
18 can be introduced as a liquid or vapor. The composition percentages of the feed  
19 components are determined by the desired operating conditions, as discussed below.

20 The fuel processor effluent stream from of the present invention includes  
21 hydrogen and carbon dioxide and can also include some water, unconverted  
22 hydrocarbons, carbon monoxide, impurities (e.g. hydrogen sulfide and ammonia) and  
23 inert components (e.g., nitrogen and argon, especially if air was a component of the feed  
24 stream).

25 Figure 1 depicts a general process flow diagram illustrating the process steps  
26 included in the illustrative embodiments of the present invention. One of skill in the art  
27 should appreciate that a certain amount of progressive order is needed in the flow of the  
28 reactants through the reactors disclosed herein.

29 Process step A is an autothermal reforming process in which two reactions, partial  
30 oxidation (formula I, below) and optionally also steam reforming (formula II, below), are  
31 combined to convert the feed stream F into a synthesis gas containing hydrogen and

1 carbon monoxide. Formulas I and II are exemplary reaction formulas wherein methane is  
2 considered as the hydrocarbon:



5 The partial oxidation reaction occurs very quickly to the complete conversion of  
6 oxygen added and produces heat. The steam reforming reaction occurs slower and  
7 consumes heat. A higher concentration of oxygen in the feed stream favors partial  
8 oxidation whereas a higher concentration of water vapor favors steam reforming.  
9 Therefore, the ratios of oxygen to hydrocarbon and water to hydrocarbon become  
10 characterizing parameters. These ratios affect the operating temperature and hydrogen  
11 yield.

12 The operating temperature of the autothermal reforming step can range from  
13 about 550°C to about 900°C, depending on the feed conditions and the catalyst. The  
14 invention uses a catalyst bed of a partial oxidation catalyst with or without a steam  
15 reforming catalyst. The catalyst may be in any form including pellets, spheres, extrudate,  
16 monoliths, and the like. Partial oxidation catalysts should be well known to those with  
17 skill in the art and are often comprised of noble metals such as platinum, palladium,  
18 rhodium, and/or ruthenium on an alumina washcoat on a monolith, extrudate, pellet or  
19 other support. Non-noble metals such as nickel or cobalt have been used. Other  
20 washcoats such as titania, zirconia, silica, and magnesia have been cited in the literature.  
21 Many additional materials such as lanthanum, cerium, and potassium have been cited in  
22 the literature as “promoters” that improve the performance of the partial oxidation  
23 catalyst.

24 Steam reforming catalysts should be known to those with skill in the art and can  
25 include nickel with amounts of cobalt or a noble metal such as platinum, palladium,  
26 rhodium, ruthenium, and/or iridium. The catalyst can be supported, for example, on  
27 magnesia, alumina, silica, zirconia, or magnesium aluminate, singly or in combination.  
28 Alternatively, the steam reforming catalyst can include nickel, preferably supported on  
29 magnesia, alumina, silica, zirconia, or magnesium aluminate, singly or in combination,  
30 promoted by an alkali metal such as potassium.

1       Process step B is a cooling step for cooling the synthesis gas stream from process  
2       step A to a temperature of from about 200°C to about 600°C, preferably from about  
3       300°C to about 500°C, and more preferably from about 375°C to about 425°C, to  
4       optimize the temperature of the synthesis gas effluent for the next step. This cooling may  
5       be achieved with heat sinks, heat pipes or heat exchangers depending upon the design  
6       specifications and the need to recover / recycle the heat content of the gas stream. One  
7       illustrative embodiment for step B is the use of a heat exchanger utilizing feed stream F  
8       as the coolant circulated through the heat exchanger. The heat exchanger can be of any  
9       suitable construction known to those with skill in the art including shell and tube, plate,  
10      spiral, etc. Alternatively, or in addition thereto, cooling step B may be accomplished by  
11      injecting additional feed components such as fuel, air or water. Water is preferred  
12      because of its ability to absorb a large amount of heat as it is vaporized to steam. The  
13      amounts of added components depend upon the degree of cooling desired and are readily  
14      determined by those with skill in the art.

15      Process step C is a purifying step. One of the main impurities of the hydrocarbon  
16      stream is sulfur, which is converted by the autothermal reforming step A to hydrogen  
17      sulfide. The processing core used in process step C preferably includes zinc oxide and/or  
18      other material capable of absorbing and converting hydrogen sulfide, and may include a  
19      support (e.g., monolith, extrudate, pellet etc.). Desulfurization is accomplished by  
20      converting the hydrogen sulfide to water in accordance with the following reaction  
21      formula III:

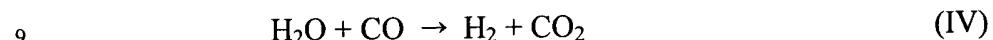


23      Other impurities such as chlorides can also be removed. The reaction is  
24      preferably carried out at a temperature of from about 300°C to about 500°C, and more  
25      preferably from about 375°C to about 425°C. Zinc oxide is an effective hydrogen sulfide  
26      absorbent over a wide range of temperatures from about 25°C to about 700°C and affords  
27      great flexibility for optimizing the sequence of processing steps by appropriate selection  
28      of operating temperature.

29      The effluent stream may then be sent to a mixing step D in which water is  
30      optionally added to the gas stream. The addition of water lowers the temperature of the  
31      reactant stream as it vaporizes and supplies more water for the water gas shift reaction of

1 process step E (discussed below). The water vapor and other effluent stream components  
2 are mixed by being passed through a processing core of inert materials such as ceramic  
3 beads or other similar materials that effectively mix and/or assist in the vaporization of  
4 the water. Alternatively, any additional water can be introduced with feed, and the  
5 mixing step can be repositioned to provide better mixing of the oxidant gas in the CO  
6 oxidation step G disclosed below.

7 Process step E is a water gas shift reaction that converts carbon monoxide to  
8 carbon dioxide in accordance with formula IV:



10 This is an important step because carbon monoxide, in addition to being highly  
11 toxic to humans, is a poison to fuel cells. The concentration of carbon monoxide should  
12 preferably be lowered to a level that can be tolerated by fuel cells, typically below 50  
13 ppm. Generally, the water gas shift reaction can take place at temperatures of from  
14 150°C to 600°C depending on the catalyst used. Under such conditions, most of the  
15 carbon monoxide in the gas stream is converted in this step.

16 Low temperature shift catalysts operate at a range of from about 150°C to about  
17 300°C and include for example, copper oxide, or copper supported on other transition  
18 metal oxides such as zirconia, zinc supported on transition metal oxides or refractory  
19 supports such as silica, alumina, zirconia, etc., or a noble metal such as platinum,  
20 rhenium, palladium, rhodium or gold on a suitable support such as silica, alumina,  
21 zirconia, and the like.

22 High temperature shift catalysts are preferably operated at temperatures ranging  
23 from about 300° to about 600°C and can include transition metal oxides such as ferric  
24 oxide or chromic oxide, and optionally including a promoter such as copper or iron  
25 silicide. Also included, as high temperature shift catalysts are supported noble metals  
26 such as supported platinum, palladium and/or other platinum group members.

27 The processing core utilized to carry out this step can include a packed bed of  
28 high temperature or low temperature shift catalyst such as described above, or a  
29 combination of both high temperature and low temperature shift catalysts. The process  
30 should be operated at any temperature suitable for the water gas shift reaction, preferably  
31 at a temperature of from 150°C to about 400°C depending on the type of catalyst used.

1     Optionally, a cooling element such as a cooling coil may be disposed in the processing  
2     core of the shift reactor to lower the reaction temperature within the packed bed of  
3     catalyst. Lower temperatures favor the conversion of carbon monoxide to carbon  
4     dioxide. Also, a purification processing step C can be performed between high and low  
5     shift conversions by providing separate steps for high temperature and low temperature  
6     shift with a desulfurization module between the high and low temperature shift steps.

7                 Process step F is a cooling step performed in one embodiment by a heat  
8     exchanger. The heat exchanger can be of any suitable construction including shell and  
9     tube, plate, spiral, etc. Alternatively a heat pipe or other form of heat sink may be  
10    utilized. The goal of the heat exchanger is to reduce the temperature of the gas stream to  
11    produce an effluent having a temperature preferably in the range of from about 90°C to  
12    about 150°C.

13                 Oxygen is added to the process in step F. The oxygen is consumed by the  
14     reactions of process step G described below. The oxygen can be in the form of air,  
15     enriched air, or substantially pure oxygen. The heat exchanger may by design provide  
16     mixing of the air with the hydrogen rich gas. Alternatively, the embodiment of process  
17     step D may be used to perform the mixing.

18                 Process step G is an oxidation step wherein almost all of the remaining carbon  
19     monoxide in the effluent stream is converted to carbon dioxide. The processing is carried  
20     out in the presence of a catalyst for the oxidation of carbon monoxide and may be in any  
21     suitable form, such as pellets, spheres, monolith, etc. Oxidation catalysts for carbon  
22     monoxide are known and typically include noble metals (e.g., platinum, palladium)  
23     and/or transition metals (e.g., iron, chromium, manganese), and/or compounds of noble  
24     or transition metals, particularly oxides. A preferred oxidation catalyst is platinum on an  
25     alumina washcoat. The washcoat may be applied to a monolith, extrudate, pellet or other  
26     support. Additional materials such as cerium or lanthanum may be added to improve  
27     performance. Many other formulations have been cited in the literature with some  
28     practitioners claiming superior performance from rhodium or alumina catalysts.  
29     Ruthenium, palladium, gold, and other materials have been cited in the literature as being  
30     active for this use.

1 Two reactions occur in process step G: the desired oxidation of carbon monoxide  
2 (formula V) and the undesired oxidation of hydrogen (formula VI) as follows:



5 The preferential oxidation of carbon monoxide is favored by low temperatures. Since  
6 both reactions produce heat it may be advantageous to optionally include a cooling  
7 element such as a cooling coil disposed within the process. The operating temperature of  
8 process is preferably kept in the range of from about 90°C to about 150°C. Process step  
9 G preferably reduces the carbon monoxide level to less than 50 ppm, which is a suitable  
10 level for use in fuel cells, but one of skill in the art should appreciate that the present  
11 invention can be adapted to produce a hydrogen rich product with of higher and lower  
12 levels of carbon monoxide.

13        The effluent exiting the fuel processor is a hydrogen rich gas containing carbon  
14        dioxide and other constituents which may be present such as water, inert components  
15        (e.g., nitrogen, argon), residual hydrocarbon, etc. Product gas may be used as the feed for  
16        a fuel cell or for other applications where a hydrogen rich feed stream is desired.  
17        Optionally, product gas may be sent on to further processing, for example, to remove the  
18        carbon dioxide, water or other components.

19 In one illustrative embodiment of the present invention, the fuel processor is of  
20 modular construction with individual modular units, which are separable, rearrangeable,  
21 and individually replaceable. The modular units may be used in any orientation, e.g.,  
22 vertical or horizontal orientation, and is adapted to be used in conjunction with a fuel cell  
23 such that the hydrogen rich product gas of the reactor described herein is supplied  
24 directly to a fuel cell as a feed stream. While the modules can have any cross sectional  
25 configuration, such as circular, rectangular, triangular, etc., a circular cross section is  
26 preferred with the overall reactor being of a generally tubular shape.

27 The modules are constructed in accordance with the description given below. The  
28 modules can be fabricated from any material capable of withstanding the operating  
29 conditions and chemical environment of the reactions described herein and can include,  
30 for example, stainless steel, Inconel, Incoloy, Hastelloy, and the like. The reaction  
31 pressure is preferable from about 0 to about 100 psig, although higher pressures may be

1 employed. The operating pressure of the fuel processor depends upon the delivery  
2 pressure required by the fuel cell. For fuel cells operating in the 1 to 20 kW range an  
3 operating pressure of 0 to about 100 psig is generally sufficient. The modules are of such  
4 dimensions so as to safely contain the reaction at the desired operating pressures and  
5 temperatures.

6 Depicted in Figure 2 is one illustrative embodiment of the present invention in  
7 which a single stack of nested reactors is utilized as a fuel processor. Fuel feed stream  
8 100 is preheated in a first heat exchanger 102 which is heated by the catalytic combustion  
9 of the anode tail gas 104 generated by a fuel cell in the anode tail gas oxidation reactor  
10 106. The catalytic combustion reaction is carried out in the anode tail gas oxidation  
11 reactor using a suitable supported catalyst. Such supported catalysts oxidation are well  
12 known in the art and may be in any suitable form, such as pellets, spheres, monolith, etc.  
13 Oxidation catalysts for carbon monoxide are known and typically include noble metals  
14 (e.g., platinum, palladium) and/or transition metals (e.g., iron, chromium, manganese),  
15 and/or compounds of noble or transition metals, particularly oxides. A preferred  
16 oxidation catalyst is platinum on an alumina washcoat. The washcoat may be applied to  
17 a monolith, extrudate, pellet or other support. Additional materials such as cerium or  
18 lanthanum may be added to improve performance. Many other formulations have been  
19 cited in the literature with some practitioners claiming superior performance from  
20 rhodium or alumina catalysts. Ruthenium, palladium, gold, and other materials have  
21 been cited in the literature as being active for this use. Thus hot exhaust 108 generated  
22 by the catalytic oxidation of the anode tail gas pre-heats the fuel to give a preheated fuel  
23 feed 112. The pre-heated fuel feed is passed through a first desulfurization unit 114 so as  
24 to substantially remove any sulfur containing compounds from the fuel. The desulfurized  
25 fuel 116 is then combined with air or another suitable oxygen source 118 and water /  
26 steam 120 to form a fuel / air / water mixture 122. The fuel / air / water mixture is  
27 introduced into the reformation stack, distributed and pre-heated in the distribution  
28 manifold. The preheated fuel / air / water mixture is introduced into the auto-thermal  
29 reformation reactor 126 and undergoes reformation into a hydrogen containing gas. The  
30 hydrogen containing gas is first cooled by a second heat exchanger 128 and then  
31 desulfurized in the second desulfurization reactor 130. The resulting desulfurized

1 hydrogen containing gas is then subjected to a water-gas shift reaction in the shift reactor  
2 132. The hydrogen containing gas exiting the shift reactor 132 is cooled by a third heat  
3 exchanger 134 and then combined with an oxygen source, such as air source 138, and  
4 then passed through a preferential oxidation reactor 136 so as to substantially remove  
5 trace amounts of carbon monoxide that may be present in the hydrogen containing gas.  
6 The hydrogen containing gas exiting the preferential oxidation reactor is subjected to  
7 cooling in a fourth heat exchanger 140 before exiting the reactor as hydrogen rich gas  
8 142. The hydrogen containing gas is preferably used in a fuel cell or may be stored or  
9 used in other processes that should be apparent to one of skill in the art.

10 Upon careful examination of Figure 2, one of skill in the art should note that  
11 except for the first desulfurization step, substantially all of the reactors in the fuel  
12 processor are nested one inside the other. The order of nesting as illustrated is designed  
13 so as to maximize the heat exchange between exothermic reactors and endothermic  
14 reactors. Thus the nested reactors achieve an optimized thermal exchange balance that  
15 optimizes the efficiency of the fuel processor in an overall compact area. In order to  
16 start-up the fuel reformer, electric pre-heater 110 may be used to pre-heat anode tail gas  
17 or some other suitable alternative startup fuel to initiate the reaction within the anode tail  
18 gas oxidation reactor. It should also be noted that the general flow of reactants through  
19 the fuel processor is proceeding from an inner core reactor to outer surrounding reactors  
20 in a "radial manner". A similar result may also be achieved by use of partially porous  
21 reactor walls made of refractory materials.

22 One of skill in the art after reviewing the above description should understand and  
23 appreciate that each module performs a separate operational function and is generally  
24 configured as shown in Figure 2. Feed stream F (100) is introduced through inlet pipe  
25 (not shown) and product gas P (142) is drawn off via outlet pipe (not shown). Module  
26 126 is the autothermal-reforming module corresponding to process step A of Figure 1.  
27 The autothermal-reforming module has built into it a heat exchanger 128 that cools the  
28 outgoing product gas which corresponds to process step B of Figure 1. Module 130 is a  
29 purifying module corresponding to process step C of Figure 1. Module 132 is a water gas  
30 shift module corresponding to process step E of Figure 1. The cooling step corresponding  
31 to process step F of Figure 1 is carried out by vertical finned heat exchanger 134.

1      Module 136 is a preferential oxidation step corresponding to process step G of Figure 1.  
2      Air source 138 provides a source for oxygen to process gas for the oxidation reaction  
3      (Equation V) of Module 136. Module 136 also contains a heat exchanger 140 (partially  
4      shown) positioned within or surrounding the catalyst bed so as to maintain a desired  
5      oxidation reaction temperature. One of skill in the art should appreciate that the process  
6      configuration described in this embodiment may vary depending on numerous factors,  
7      including but not limited to feedstock quality and required product quality.

8              Turning now to Figure 3, an alternative illustrative embodiment of a dual stack  
9      fuel processor is shown in which there is a reforming stack 30 and a oxidizing stack 40.  
10     As will become apparent below, the reforming stack 30 generally carries out the  
11    reformation process in which fuel is converted into suitably pure hydrogen gas for use  
12    with a fuel cell (not shown). The oxidation stack generally serves as a means for  
13    recovering the heat content of the anode tail gas generated by the fuel cell and preheats  
14    the fuel for the reforming stack.

15              Fuel 200 is provided to the reforming stack 40 that includes two major  
16    components, the anode tail gas oxidation reactor 204 and the desulfurization reaction 210.  
17    The anode tail gas oxidation reactor is designed such that it catalytically oxidizes the  
18    anode tail gas 206 generated from a fuel cell. The heat generated is transferred to the fuel  
19    200 by vertical fin heat exchangers 202 generating a cooled exhaust 208. The heated fuel  
20    is then subjected to a desulfurization reactor 210 that substantially removes the sulfur  
21    compounds present in the fuel. The desulfurized fuel 212 is provided to the reforming  
22    stack 30 and combined with air 214 and hot water / steam 216. This mixture of fuel / air /  
23    water passes through a distribution manifold 218 which directs the mixture through a  
24    vertical fin heat exchanger 220. The pre heated fuel / air / water mixture is then  
25    introduced into the auto-thermal reformation reactor 224. During start-up, an electrical  
26    pre-heater element 222 is installed at the bottom of the auto-thermal reformation reactor.  
27    However, once started the heat generated by the auto-thermal reformation reactor is  
28    sufficient to heat the fuel / air / water mixture via the vertical finned heat exchangers 220.  
29    The product gas from the auto-thermal reforming reactor is directed to a second  
30    desulfurization reactor 226 which removes any remaining sulfur compounds from the gas  
31    product stream. The desulfurized gas is then introduced into the water-gas shift reactor

1 228. The temperature of the shift reactor is controlled by tube heat exchangers 232. It  
2 should be noted at this point that the heat exchanger in the present illustrative  
3 embodiment is designed as one continuous tube routed throughout the reforming stack.  
4 Points A and B are respectively connected to each other such that the flow of water  
5 through the tube is continuous. After passing through the shift reactor, air 229 is mixed  
6 with the hydrogen containing gas and passed to a preferential oxidation reactor 230. In  
7 the preferential oxidation reactor trace amounts of carbon monoxide are removed so as to  
8 purify the hydrogen containing gas for use in a fuel cell. The product gas is further  
9 cooled by heat exchanger coils 232 and leaves the reforming stack as hydrogen  
10 containing gas 236. The hydrogen containing gas is preferably used in a fuel cell or may  
11 be stored or used in other processes that should be apparent to one of skill in the art.

12 One of skill in the art after reviewing the above description of Figure 3 should  
13 understand and appreciate that each module performs a separate operational function.  
14 Feed stream F (200) is introduced through inlet pipe (not shown) and product gas P (236)  
15 is drawn off via outlet pipe (not shown). Module 224 is the autothermal reforming  
16 module corresponding to process step A of Figure 1. The autothermal reforming module  
17 has built into it a vertical fin heat exchanger the simultaneously heats the incoming fuel  
18 mixture and cools the outgoing product gas which corresponds to process step B of  
19 Figure 1. An electric heater 222, is installed at the bottom inlet of the autothermal  
20 reformation reactor for start-up heat. Module 226 is a purifying module corresponding to  
21 process step C of Figure 1. Module 228 is a water gas shift module corresponding to  
22 process step E of Figure 1. The cooling step corresponding to process step F of Figure 1  
23 is carried out by finned tube heat exchanger 232. In this illustrative embodiment, heat  
24 exchanger 232 is shown as a general heat sink for the entire reforming stack, however,  
25 one of skill in the art could redesign the heat exchangers to have multiple flows and heat  
26 exchangers. Module 230 is an oxidation step corresponding to process step G of Figure  
27 1. Air source 229 provides a source for oxygen to process gas for the oxidation reaction  
28 (Equation V) of Module 230. Module 230 also contains a heat exchanger 232 (partially  
29 shown) positioned within or surrounding the catalyst bed so as to maintain a desired  
30 oxidation reaction temperature. One of skill in the art should appreciate that the process

1 configuration described in this embodiment may vary depending on numerous factors,  
2 including but not limited to feedstock quality and required product quality.

3 In view of the above disclosure, one of ordinary skill in the art should understand  
4 and appreciate that the present invention includes many possible illustrative embodiments  
5 that depend upon design criteria. One such illustrative embodiment includes a compact  
6 fuel processor for converting a hydrocarbon fuel feed into hydrogen rich gas, in which  
7 the fuel processor assembly includes multiple concentric vessels for converting the  
8 hydrocarbon fuel feed into the hydrogen rich gas. The hydrogen rich gas thus generated  
9 is suitable for direct feed to a fuel cell or may be stored for use later or may be used in  
10 processes or reactions that utilize hydrogen gas as a feed stock.

11 In such an illustrative embodiment, the processor assembly itself includes: an  
12 oxidation core vessel containing an oxidation catalyst; a reforming vessel surrounding the  
13 oxidation core vessel and forming a first annular space filled with autothermal reforming  
14 catalyst; a desulfurizing vessel surrounding the reforming vessel and forming a second  
15 annular space filled with desulfurization catalyst; a shift vessel surrounding the  
16 desulfurizing vessel and forming a third annular space filled with water gas shift catalyst;  
17 and a preferred oxidation vessel surrounding the shift vessel and forming a fourth annular  
18 space filled with preferred oxidation catalyst. The above reactor areas, except for the  
19 oxidation core vessel, are in fluid communication with each other so as to carry out the  
20 desired fuel processing reactions needed to generate substantially pure hydrogen gas.  
21 The oxidation core vessel oxidizes fuel cell anode tail gas or alternatively another  
22 suitable fuel such as natural gas, to produce a hot exhaust gas. The hot exhaust gas in  
23 turn preheats the hydrocarbon fuel that is utilized in the fuel reformation reactions. In  
24 one preferred illustrative embodiment, an electric heater is present for preheating the  
25 anode tail gas prior to introducing the anode tail gas to the oxidation core vessel. The  
26 illustrative compact fuel processor may include an external desulfurizing vessel for  
27 desulfurizing the hydrocarbon fuel feed. Preferably the second desulfurizing vessel is a  
28 replaceable canister so that it is serviceable without having to disassemble the nested fuel  
29 processor stack. In the present illustrative embodiment, the hydrocarbon fuel feed is  
30 sequentially introduced to the first annular space, then to the second annular space, then  
31 to the third annular space, and then to the fourth annular space to produce the hydrogen

1 rich gas. A plurality of cooling coils for removing the heat of reaction produced in the  
2 first annular space, the second annular space, the third annular space, and the fourth  
3 annular space are preferably employed in the illustrative embodiment so as to efficiently  
4 distribute the heat generated by the exothermic reaction and the heat requirements of the  
5 endothermic reactions. A circulating coolant flows through the cooling coils and  
6 preferably the circulating coolant is selected from air, water, the hydrocarbon fuel feed,  
7 combinations and mixtures of these and similar items. In one preferred illustrative  
8 embodiment each annular space is surrounded by heat resisting refractory. Thus the heat  
9 transfer between annular spaces is controlled and the overall heat efficiency of the fuel  
10 processor can be optimized.

11 Yet another illustrative embodiment of the present invention is a compact fuel  
12 processor for converting a hydrocarbon fuel feed into hydrogen rich gas, that includes a  
13 heat exchanger coil; a reforming core vessel containing an autothermal reforming catalyst  
14 bed; a desulfurizing vessel surrounding the reforming core vessel and forming a first  
15 annular space filled with desulfurization catalyst; a shift vessel surrounding the  
16 desulfurizing vessel and forming a second annular space filled with water gas shift  
17 catalyst; and a preferred oxidation vessel surrounding the shift vessel and forming a third  
18 annular space filled with preferred oxidation catalyst. Such an illustrative compact fuel  
19 processor is designed such that the hydrocarbon fuel feed is preheated by the hydrogen  
20 rich gas in the heat exchanger coil to produce a preheated hydrocarbon fuel feed; and the  
21 preheated hydrocarbon fuel feed is sequentially introduced to the reforming core vessel,  
22 then to the second annular space, then to the third annular space, and then to the fourth  
23 annular space to produce the hydrogen rich gas.

24 It is preferred within this illustrative embodiment that the reforming core vessel  
25 has a set of external vertical fins for further preheating the preheated hydrocarbon fuel  
26 feed to produce a second preheated hydrocarbon fuel feed. Thus, the second preheated  
27 hydrocarbon fuel feed becomes the preheated hydrocarbon fuel feed introduced to the  
28 reforming core vessel. It should also be noted that the second annular space may have a  
29 second heat exchanger coil for reaction temperature control. Further the present  
30 illustrative embodiment can include an electrical heater for starting up the autothermal  
31 reforming catalyst bed.

1        While the apparatus, compositions and methods of this invention have been  
2 described in terms of preferred or illustrative embodiments, it will be apparent to those of  
3 skill in the art that variations may be applied to the process described herein without  
4 departing from the concept and scope of the invention. All such similar substitutes and  
5 modifications apparent to those skilled in the art are deemed to be within the scope and  
6 concept of the invention as it is set out in the following claims.